# <u>Alkene Hydrogenation</u> (Dihydride Intermediate)



- [RhCl(PPh<sub>3</sub>)<sub>3</sub>] (Wilkinson's Catalyst)
- [{Rh(NBD)(m-Cl)}<sub>2</sub>] + 4 PR<sub>3</sub> or [{Ir(COD)(m-Cl)}<sub>2</sub>] + 4 PR<sub>3</sub>
- [Ir(COD)(PMePh<sub>2</sub>)<sub>2</sub>][PF<sub>6</sub>] or [Ir(COD)(PCy<sub>3</sub>)(Py)][PF<sub>6</sub>]
- [Rh(NBD)(bidentate phosphine)][PF<sub>6</sub>]

- (NBD = norbornadiene)
- (COD = 1,5-cyclooctadiene)



- Note: Hydrogenation involves 1,2-insertion, so *syn*-addition to the alkene is observed.
- Note: Less substituted alkenes are hydrogenated faster.

# Alkene Hydrogenation (Monohydride)



### **Asymmetric Hydrogenation**



- Two enantiomers may be formed from a prochiral alkene (or ketone or imine)
- With a suitable chiral metal complex, the alkene will bind predominantly through one face.
  This is the face that is hydrogenated, giving predominantly a single enantiomer.
- Asymmetric hydrogenation is possible because the last step of the catalytic cycle is irreversible → kinetic products.
- 2001 Nobel Prize for William Knowles and Royoji Noyori.



## **Asymmetric Hydrogenation**



# **Hydrogenation**

#### What about other substrates?

The C=O and C=N bonds of ketones and imines are only reduced by certain catalysts {e.g. [M(diphosphine)]+ (M = Rh or Ir), [RuCl<sub>2</sub>(diphosphine)] or [CpRe(CO)(PPh<sub>3</sub>)]<sup>+</sup>}



- Aryl rings are NOT reduced by the usual catalysts (see below).
- CN, NO<sub>2</sub>, ester or amide groups are NOT reduced by the usual catalysts.

#### Arene Hydrogenation

- Several heterogeneous catalysts can do this (*e.g.* Rh/C)
- None of the catalysts discussed so far will hydrogenate arenes



## Monsanto Acetic Acid Process



- Used to produce 3.8 million tonnes of MeCO<sub>2</sub>H p.a. Most of this acetic acid is converted to acetic anhydride (used in the synthesis of cellulose acetate and asparin, *etc.*). Eastman has a similar process to the Monsanto process which produces acetic anhydride directly.
- Monsanto acetic acid process runs at 180 °C and 30-40 atm of CO.
- Rate determining step is oxidative addition of MeI.

### **Olefin Hydrosilation**



- One of the earliest catalysts  $H_2$ PtCl<sub>6</sub> was (Speier's Catalyst) originally thought to be homogeneous but more likely that catalysis is due colloidal platinum to metal.
- Homogeneous catalysts include  $Co_2(CO)_8$ ,  $Ni(COD)_2$ ,  $NiCl_2(PPh_3)_2$  and RhCl(PPh<sub>3</sub>)<sub>3</sub>

## **Co-Catalyzed Alkene Hydroformylation**



# **Alkene Hydroformylation**

#### Problems with the cobalt catalyzed hydroformylation reaction:

- Ratio of linear to branched aldehydes is 4:1 at best.
- Catalyst is unstable, so its separation and recovery are difficult
- High temperature (140-180 °C) and pressure (200-300 atm) of CO required  $\rightarrow$  plants are expensive to build and operate

#### $HRh(CO)(PPh_3)_3$ has many advantages over cobalt catalysts:

- 100 to 1000 times more active
- Pressure (15 to 25 atm) and temperature (80 to 120 °C) are much lower than needed for cobalt catalysts (200-300 atm and 140-180 °C).
- Linear to branched ratios as high as 14:1 are obtained. Only the linear product is commercially valuable.
- HRh(CO)(PPh<sub>3</sub>)<sub>3</sub> is also an excellent isomerization catalyst. Therefore, in the hydroformylation of H<sub>2</sub>C=CH–CH<sub>2</sub>–Me or Me–CH=CH–Me, the major product is Me–CH<sub>2</sub>–CH<sub>2</sub>–CH<sub>2</sub>–CHO.
- Advantages far outweigh the drawback of having to recover the expensive Rh catalyst {rhodium is 500 to 5000 times more expensive than cobalt (depends on the year)}.

## **Rh-Catalyzed Alkene Hydroformylation**

